

AMENDMENTS

In the Specification:

In the disclosure as published, replace paragraph [0064] as shown hereinafter:

Marked-Up Version

[0064] The separator packings (33a, 33b) allow to avoid that the large drops flow into a further bed. With the vessels systems from prior art, there is [[an]] a higher risk that a coalesced large drop enters the further bed. If some large drops enters enter the further bed, an efficiency of the vessel system to separate droplets from the continuous phase may be considerably reduced. Consequently, the ~~vessels~~ vessel systems from prior art comprises [[an]] a high number of beds so as to insure that a given dispersed phase content in the purified fluid is achieved. The ~~vessels~~ vessel systems according to the present invention hence allow to provide a lower number of beds to achieve the given dispersed phase content in the purified fluid. Typically, in a case of produced water to be purified, a vessel system according to the present invention comprising eight beds produces a purified fluid having an oil content lower than 15 ppm, whereas in prior art, such oil content is provided with a vessel system comprising twelve beds.

Clean Version

[0064] The separator packings (33a, 33b) allow to avoid that the large drops flow into a further bed. With the vessels systems from prior art, there is a higher risk that a coalesced large drop enters the further bed. If some large drops enter the further bed, an efficiency of the vessel system to separate droplets from the continuous phase may be considerably reduced. Consequently, the vessel systems from prior art comprises a high number of beds so as to insure that a given dispersed phase content in the purified fluid is achieved. The vessel systems according to the present invention hence allow to provide a lower number of beds to achieve the given dispersed phase content in the purified fluid. Typically, in a case of produced water to be purified, a vessel system according to the present invention comprising eight beds produces a purified fluid having an oil content lower than 15 ppm, whereas in prior art, such oil content is provided with a vessel system comprising twelve beds.

In the disclosure as published, replace the ABSTRACT as shown hereinafter:

Marked-Up Version

A system for separating an emulsion fluid into a recovered fluid and a purified fluid. The emulsion fluid comprises a continuous phase and a dispersed phase. The purified fluid is essentially constituted of the continuous phase. The system comprises a vessel at an inlet of which the emulsion fluid may flow. The system further comprises one or more coalescing ~~element~~ elements made of Reusable Polymer Absorbent material. Each coalescing element allows to coalesce at least a portion of the dispersed phase from small droplets into large drops further detached from the coalescing element upon a flow of the emulsion fluid. The system further comprises one or more separating and guiding ~~[[mean]]~~ means made of oleophilic material. Each separating and guiding ~~[[mean]]~~ means is located a distance from an associated ~~with one~~ coalescing element and is disposed at an output of the associated coalescing element to guide the detached large drops for further recovery. The separating and guiding means has a structure that is adapted to allow the continuous phase to flow through the separating and guiding means.

Clean Version

A system for separating an emulsion fluid into a recovered fluid and a purified fluid. The emulsion fluid comprises a continuous phase and a dispersed phase. The purified fluid is essentially constituted of the continuous phase. The system comprises a vessel at an inlet of which the emulsion fluid may flow. The system further comprises one or more coalescing elements made of Reusable Polymer Absorbent material. Each coalescing element allows to coalesce at least a portion of the dispersed phase from small droplets into large drops further detached from the coalescing element upon a flow of the emulsion fluid. The system further comprises one or more separating and guiding means made of oleophilic material. Each separating and guiding means is located a distance from an associated coalescing element and is disposed at an output of the associated coalescing element to guide the detached large drops for further recovery. The separating and guiding means has a structure that is adapted to allow the continuous phase to flow through the separating and guiding means.